

AMENDMENTS TO THE CLAIMS

This listing of claims will replace all prior versions and listings of claims in the application:

LISTING OF CLAIMS:

1. (Original) A method for producing a purified 2-cyanoacrylate by distilling a crude 2-cyanoacrylate in the presence of a polymerization inhibitor, characterized in that a polymerization inhibitor having a boiling point at normal pressure of within $\pm 12^{\circ}\text{C}$ of the boiling point at normal pressure of the purified 2-cyanoacrylate is used as the polymerization inhibitor.
2. (Original) The production method according to Claim 1, wherein the polymerization inhibitor is an anionic polymerization inhibitor.
3. (Original) The production method according to Claim 2, wherein the anionic polymerization inhibitor is a halocarboxylic acid or a halosulfonic acid.
4. (Original) The production method according to Claim 3, wherein the halocarboxylic acid or the halosulfonic acid is chloroacetic acid, dichloroacetic acid, trichloroacetic acid, bromoacetic acid, dibromofluoroacetic acid, 3-chloropropionic acid, 2,2-dichloropropionic acid, 2-bromopropionic acid, 2-chlorobutyric acid, 4-chlorobutyric acid, pentafluoropropanesulfonic acid, nonafluorobutanesulfonic acid, trichloroacrylic acid, undecafluoropentanesulfonic acid, tridecafluorohexanesulfonic acid, or 3-methylsulfanylpropionic acid.
5. (Original) The production method according to Claim 2, wherein the anionic polymerization inhibitor is a BF_3 methanol complex or a BF_3 ethanol complex.
6. (Original) The production method according to Claim 1, wherein the polymerization inhibitor is added to a vessel in advance.

7. (Original) The production method according to Claim 1, wherein the polymerization inhibitor is dissolved in a purified 2-cyanoacrylate and continuously added via an upper part of a distillation vessel or an upper part of a distillation column.
8. (Original) The production method according to Claim 6, wherein the polymerization inhibitor is added at 1 to 1000 wt ppm relative to the crude 2-cyanoacrylate.
9. (Original) The production method according to Claim 7, wherein the polymerization inhibitor is added at 1 to 1000 wt ppm relative to the crude 2-cyanoacrylate.
10. (Currently Amended) The production method according to ~~any one of~~ Claims 1 ~~to 9~~, wherein a crude 2-cyanoacrylate obtained by heating and condensing a cyanoacetic acid ester and formaldehyde in an organic solvent in the presence of a basic catalyst, and depolymerizing the condensate thus obtained in the presence of a depolymerization catalyst and a polymerization inhibitor at reduced pressure and high temperature is used as the crude 2-cyanoacrylate.
11. (Currently Amended) The production method according to ~~any one of~~ Claims 1 ~~to 9~~, wherein distillation employs a method in which heating is carried out at reduced pressure using a packed distillation column.
12. (Currently Amended) The production method according to ~~any one of~~ Claims 1 ~~to 9~~, wherein distillation is carried out by further adding, to a 2-cyanoacrylate in a vessel, an anionic polymerization inhibitor and a radical polymerization inhibitor that have a boiling point that is higher than the boiling point of the 2-cyanoacrylate by more than 12°C.
13. (Original) The production method according to Claim 12, wherein the anionic polymerization inhibitor is phosphorus pentoxide and the radical polymerization inhibitor is hydroquinone.